### Speeding Carbon Dioxide Capture -The Key to Better Energetics

#### Lawrence Livermore National Laboratory



University of Illinois, Urbana-Champaign



The Babcock and Wilcox Company

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George Farthing Babcock and Wilcox

Jennifer Lewis, University of Illinois

Carbonic anhydrase is one of the most rapid enzymes known - it was first discovered in human lungs, where it facilitates CO<sub>2</sub> exhalation

Carbonic anhydrase appears to have evolved independently five times, and has hundreds of structural variants





## The problem for today – carbon dioxide separation is too slow

- Separating pure CO<sub>2</sub> from industrial sources, or from the atmosphere, is a slow chemical reaction
- This requires large process equipment and long times, leading to high costs
  - Separation from natural gas power is 3-4x slower than coal
  - Separation from air is 300x slower than from coal flue gas
- Water-based liquids separate CO<sub>2</sub> from other gases with very high efficiency because CO<sub>2</sub> is very soluble in water



## We have focused on using natural analgues to beat the speed limit

- Faster, rugged catalysts that survive industrial conditions
- Tethering of catalysts to the air-water interface
- Encapsulation to provide high surface area and confine solvent







## And we are examining processes that utilize solid bicarbonate



25% exchangeable CO<sub>2</sub> by weight



### The transfer of $CO_2$ into water or other liquids is almost always dominated by chemical reactions at the liquid interface



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**First we want a general approach for mimicking enzymes** with small molecules - then to apply it to CO<sub>2</sub> capture

CA Structure & Function: His triad, axial –OH, coordinate  $Zn^{2+}$  center, key amino acids bind  $CO_2$ 

Mimics: optimize metal and ligand identity to improve kinetics Carbonic Anhydrase



### Zn<sup>2+</sup>/His triad active site

### We have created mimic catalysts that they are stable at 100°C, and their rate increases with temperature

Catalyst	Buffer	Temp (C)	K <sub>cat</sub>
Zn(BF <sub>4</sub> ) <sub>2</sub> ctrl	Hepes, phenol red, pH = 7.5	T <sub>r</sub>	7
Cyclen-Zn	Hepes, phenol red, pH = 7.5	T <sub>r</sub>	540
Cyclen-Zn	Hepes, phenol red, pH = 7.5	Post 18 h, 100 C	900
Cyclen-Zn	AMPSO, thymol blue, pH = 9.0	T <sub>r</sub>	2500
Cyclen-Zn	AMPSO, thymol blue, pH = 9.0	Post 18h, 100 C	2260
Cyclen-Zn	AMPSO, thymol blue	50C	11,500



Demonstrated stability and enhanced kinetics for cyclen at elevated temperature and pH conditions

## Our mimics are faster at higher temperatures



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### And stable up to at least 120°C



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The catalyst can be formed from zinc carbonate, indicating that carbonate solutions will not scavenge the zinc



## But we still have to deal with the surface transfer issue



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# The trick is tethering the catalyst to the liquid/gas interface – again nature is our example





Polyethyleneglycol (PEG) linkers do not deform the catalysts and appear to be appropriate for tethering to hydrophobic groups

PE G

> ~50 PEG units keep the catalyst removed from the immediate surface

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### Catalysis is not the only speedenhancer – surface area is critical



## We can create encapsulated solvents analogous to alveoli in size and function



**Concept**: Encapsulate liquid solvents such as MEA in a thin, permeable, polymer shell.

#### **Initial Goals**

✓ Reduced volatility

✓ Degradation products contained





**Additional Benefits** 

✓ Increased surface area

✓ Good interface with capture catalysts

 ✓ Facilitates new chemistries, especially high viscosity



### We have pursued microcapsules made from a photocurable silicone (Semicosil)



Inner fluid: 5 wt% PEO solution in water with green dye Middle fluid: Unmodified Semicosil A & B (10:1) Outer fluid:

2 wt% PVA, 34 wt% H<sub>2</sub>O, 64 wt% glycerol



### Successful fabrication of microcapsules with Semicol UV curable silicon



### Microcapsule production requires balanced fluid properties



Capillary	<b>ID (μm)</b>	OD (μm)	Fluid	Viscosity (cP)	Flow rate (µl h <sup>-1</sup> )
Injection	50	1000	Inner Fluid	10-50	200-800
Collection	500	1000	Middle Fluid	10-50	200-800
Square	1000	1200	Outer Fluid	100-500	2000-3500

Formation of double emulsions within microfluidic device using methods as described by the Weitz group



## Our current process runs at 250 capsules per second – too fast for this movie!











### We have encapsulated multiple solvents in silicone capsules – with and without added catalyst





### Carbonate solvents show carbon capture amounts of over 3 moles $CO_2$ per liter of solvent (13 wt % $CO_2$ )

- Plot shows the increase in carbon content as 30 wt % (4m) Na2CO3 reacts with flue gas.
- Calculated carbon capacity is the maximum possible per 1000g H2O in solvent. Still need to get it back out.
- Most of the carbon capacity comes at PCO<sub>2</sub>>0.001.
- Nahcolite doubles carbon capacity.







Why attempt high pressure recovery with solids present?

- High PCO2
  - Less energy to compress CO2
  - Less water boiled
  - Less carbon transfer per unit of solvent
- Low PCO2
  - More energy to compress gas
  - More water boiled
  - More carbon transfer per unit of solvent





#### 30 wt % (4M) Sodium Carbonate (1) – Phase behavior





in kJ per mole of CO2 removed

## Speeding carbon dioxide absorption will enable low energy process approaches

- Faster, rugged catalysts that survive industrial conditions
- Tethering of catalysts to the air-water interface
- Encapsulation to provide high surface area and confine solvent, permit solids formation





